

Evaluating the Oxygen Reaction Rate Coefficient of Sulphidic Tailings using Laboratory and Field Tests

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Abstract

The oxygen flux into exposed tailings can be assessed in the field by conducting oxygen consumption (OC) tests. Such tests can also be conducted in the laboratory using closed cells. As shown in this paper, numerical solutions can advantageously be used to interpret OC tests and evaluate the experimental values of the diffusion (D_e) and reaction rate (K_r) coefficients. These two parameters are included in modified Fick's laws that give the oxygen flux entering the surface of reactive tailings. The paper describes both types of OC tests, as performed in the field on an abandoned tailings impoundment at the Manitou mine site in north-western Quebec and in the laboratory on the Manitou tailings. The experimental results are interpreted using numerical simulations of the tests performed with commercial codes. The values of coefficient K_r obtained in the field (under natural conditions) and in the laboratory (under preset conditions) are also compared and discussed.

Key Words: Fick's laws, oxygen diffusion, oxygen consumption, numerical simulations, surface flux

Introduction

Reclamation of tailings disposal sites containing sulphidic minerals that can oxidize to produce acid rock drainage (ARD) is a high priority for many mining operations. Engineered soil covers acting as oxygen barriers can be used for that purpose in regions with a relatively humid climate, when the water balance favors long term moisture storage (Nicholson et al. 1989, Bussière et al. 2003). Evaluation of the oxygen flux consumed by the tailings is useful to assess the efficiency of the cover, as its performance is often determined by comparing the fluxes into the reactive tailings with and without the cover. These fluxes can be obtained under transient or (pseudo) steady-state conditions using analytical (for simple boundary and initial conditions) or numerical solutions, based on the modified versions of Fick's first and second laws (Aubertin et al. 1999; Mbonimpa et al. 2003, 2011). These laws (Eqs. 1 and 2) provide a practical means to evaluate the diffusive oxygen flux $F(z, t)$ at position z and time t (Collin and Rasmussen, 1988; Nicholson et al. 1989) into reactive tailings. For a one-dimensional diffusion process, the Fick's first law can be written as (Mbonimpa et al. 2003; 2011)

$$F(z, t) = -D_e \frac{\partial C(z, t)}{\partial z} = -\theta_{eq} D^* \frac{\partial C(z, t)}{\partial z} \quad (1)$$

where D_e is the effective oxygen diffusion coefficient; $C(z, t)$ is the oxygen concentration (in the gas phase); θ_{eq} is the equivalent (diffusion) porosity. Parameter θ_{eq} takes into account the oxygen in the air and water phases (Aubertin et al. 1999, 2000), i.e. $\theta_{eq} = \theta_a + H\theta$ (where θ_a is the air filled porosity, θ is the volumetric water content; H is the dimensionless Henry's equilibrium constant - $H \cong 0.03$ at 20°C for oxygen). Parameter D^* ($= D_e / \theta_{eq}$) is the bulk diffusion coefficient.

For sulphidic minerals, it is often assumed that the diffusing oxygen is being consumed by an irreversible first-order kinetic reaction that follows an exponential decay (e.g. Elberling and Nicholson 1996). In this case, a modified version of Fick's second law can be used to evaluate the interstitial oxygen concentration

$C(z, t)$; for one-dimensional process, this equation can be expressed as follows (Mbonimpa et al. 2003; 2011).

$$\frac{\partial}{\partial t}(\theta_{eq} C) = \frac{\partial}{\partial z} \left(D_e \frac{\partial C}{\partial z} \right) - K_r C = \frac{\partial}{\partial z} \left(\theta_{eq} D^* \frac{\partial C}{\partial z} \right) - \theta_{eq} K_r^* C \quad (2)$$

In eq. 2, parameters K_r^* and $K_r (= \theta_{eq} K_r^*)$ are the bulk and effective reaction rate coefficients, respectively.

Various laboratory and field testing methods were developed to characterize reactive tailings and determine the value of parameters D_e and K_r . New interpretation procedures have been proposed by the authors for oxygen consumption tests in closed reservoirs, based on numerical simulations of the oxygen migration into reactive tailings. This paper recalls briefly the testing methodologies and interpretation procedures, and then compares the results obtained from laboratory tests carried out on tailings from the Manitou site with those obtained using field oxygen consumption (OC) tests on the Manitou site.

Site Description and Tailings Sampling

The tailings were sampled at the Manitou mine site, located about 10 km east of the city of Val-d'Or in north-western QC, Canada. The overall site plan is shown in Figure 1. During the mining operation (from 1942 to 1979), about 11 million tons of zinc, copper and lead ore were treated on this site. The tailings were first deposited in a natural valley, and later in tailings impoundments A and B (see Figure 1). Dike breaches lead to partial tailings discharge around the impoundments, while wind and water erosion contributed to further spreading. At the time of this experimental study (2006), the tailings occupied about 185 hectares on three main areas: impoundments A and B (43 ha), the original discharge area and spill zone (90 ha), and the delta along the Bourlamaque river (52 ha). The relatively coarse grained texture (sandy silt) of the tailings favors natural drainage. The water table was fairly deep (about 8 meters) in impoundment A, which was the focus of this investigation.

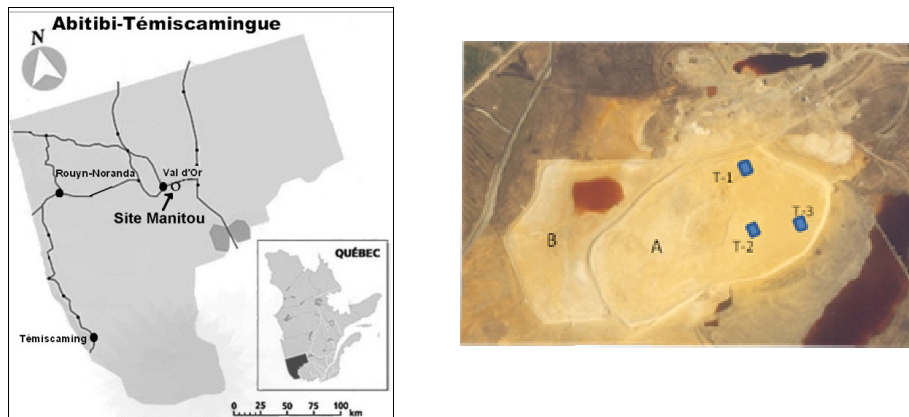


Figure 1. Plan showing the location of the Manitou mine site (left) and aerial view of the Manitou site and approximate locations of the three trenches T1 to T3 where the tailings were sampled and field OC tests performed (right).

The Quebec Ministry of Natural Resources and Fauna (MRNF) took over the site, following the bankruptcy of the mining rights owners in 2003. A progressive rehabilitation plan was about to be implemented at the time of this experimental investigation. As part of this ongoing plan, tailings from the Agnico Eagle Mines (AEM) Goldex project, located west of Val-d'Or, QC, are being used to cover the acid generating Manitou tailings; new dikes constructed on the site are also expected to raise the water table. The rehabilitation program is planned to continue for many years (Émond et al. 2011).

A sampling campaign was carried out in June 2006. Three trenches (T-1, T-2, and T-3) with a depth of 1.5 to 1.8 m were excavated in impoundment A; locations are indicated in Figure 1. Visual observations in these trenches indicated physical and chemical heterogeneities (stratifications) with variable alteration conditions. The tailings were generally more oxidized close to the surface (up to about 1.2 m deep), and remained relatively intact (grey) at larger depth. Tailings samples were collected at the bottom of each trench. The three samples were mixed to obtain a composite sample (about 240 kg). These “unoxidized” tailings were put in buckets and kept under water to minimize contact with oxygen.

Basic physical and geochemical characterisation was performed on the tailings sample. The grain-size distribution is fairly typical of hard rock tailings (sandy fraction) with a D_{10} of about 0.015 mm, D_{30} near 0.080 mm and D_{60} of 0.200 mm. According to the unified (USCS) system, these tailings are classified as silty sand (SM). The relative density of the solid particles is about 2.8. The chemical and mineralogical analysis indicated that pyrite was the main sulfide mineral, with a content of about 7% (w/w). The net neutralisation potential (NNP) is about -142 (kg CaCO_3/t), confirming the acidic nature of these tailings.

Laboratory Tests in Closed Cells

The main experimental procedure to determine parameters D_e and K_r in the laboratory is based on the oxygen diffusion and consumption (ODC) test, developed progressively over the years (Aubertin et al. 1995, 1999, 2000; Aubertin et Mbonimpa, 2001; Mbonimpa et al. 2003). This test is conducted in a closed cell with two reservoirs, initially purged with nitrogen, located on both sides of the sample. The source reservoir is then filled with air from which oxygen diffuses through the material where it is partially consumed. The flow through is collected in the receptor reservoir. The change in oxygen concentration measured directly in both reservoirs is used to obtain D_e and K_r . Such tests were included in this investigation (results not shown here) to assess materials properties and to help validate other types of measurements.

An alternative measurement method, which involves the use of a closed cell with a single reservoir, leads to a more precise determination of K_r (Gosselin 2007; Gosselin et al. 2007). This ODC test uses the experimental setup shown in Figure 2.

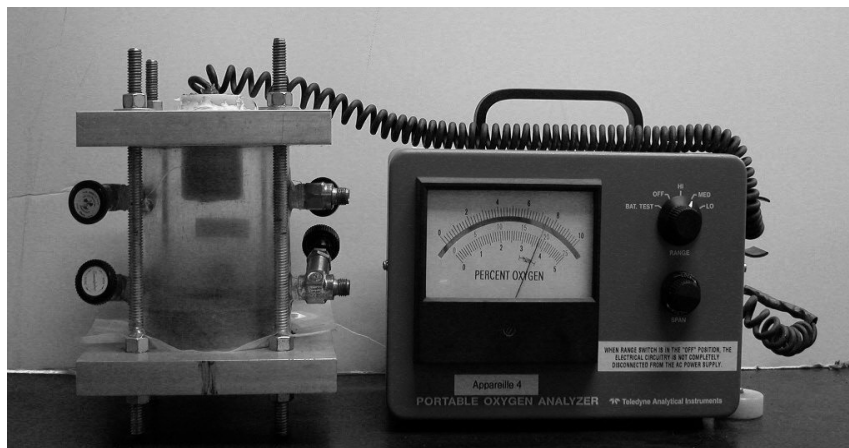


Figure 2. The laboratory ODC test cell with a single reservoir

In this case, the tailings are put in place, at the desired porosity n and water content θ , at the base of a Plexiglas cylinder with a diameter of 8 cm. The specimen thickness is about 2 cm, while the height of the reservoir above varies from 5 to 10 cm. An oxygen sensor (Teledyne 320 P/D) measures the concentration of oxygen. This sensor is calibrated for each test. Before starting a test, the cell is purged with humidified nitrogen. The cell filled with nitrogen is left standing 24 hours to make sure that it is airtight. The top reservoir is then filled with air under atmospheric conditions. Oxygen migrates inside the

tailings(due to the concentration gradient in the closed cell) where it is consumed by the oxidation of sulphidic minerals. The evolution of the oxygen concentration in the reservoir is monitored and used to back calculate the values of D_e and K_r . The test ends when the oxygen concentration has decreased significantly (i.e. down to 15 % or less). A series of 10 tests were conducted on the Manitou tailings at various degrees of saturation (S_r). The tailings (initially kept under water) were previously dried under a nitrogen atmosphere before the first test.

The interpretation approach for the laboratory ODC and OC tests is based on numerical solutions to the modified Fick's law presented above (e.g. Mbonimpa et al. 2003, 2011). The software POLLUTE (Rowe et al. 1994) was used for the numerical simulations of these tests. POLLUTE has been used for many years to simulate oxygen diffusion in unsaturated media. The evolution of the oxygen concentration in the reservoir(s) is calculated for given (preset) values of D^* and K_r^* . Iterative calculations are performed to adjust the calculated and measured oxygen concentrations and thus obtain the most representative values of D^* and K_r^* (and the corresponding values of D_e and K_r). This approach assumes that the material characteristics (volumetric water content θ , porosity n , D_e and K_r) are uniform and constant during a test.

Field OC Tests

Seven field OC tests were carried out on the Manitou tailings site, following the approach proposed by Elberling et al. (1994, 1996), and illustrated schematically in Figure 3. These authors have demonstrated the use of the field oxygen consumption (OC) test to estimate the steady-state surface oxygen flux into tailings exposed to the atmosphere. The test consists of driving an aluminum cylinder into the tailings, leaving an empty space at the top that forms the oxygen reservoir (by closing the cylinder with a tight lid). The progressive decrease of oxygen concentration in the closed chamber is monitored over time, i.e. $C(z=0, t>0)$, where z is the depth from the surface of the tailings. The initial oxygen concentration $C(z=0, t=0) = C_0$ corresponds to the atmospheric concentration ($C_0 = 20.9\%$ or about 8.65 mole/m^3 or 276 g/m^3).

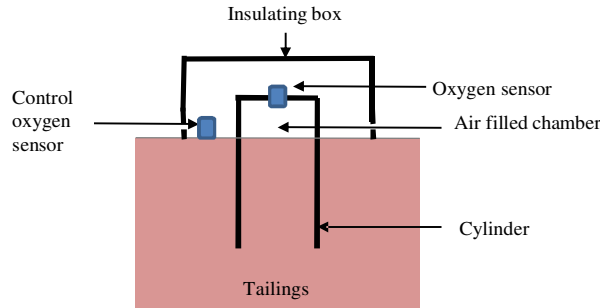


Figure 3. Schematic view of a vertical section for a typical setup of the field OC test.

A conventional (analytical) interpretation approach was used by Elberling et al. (1994) for short duration OC tests, assuming that a steady-state condition existed before the test and was maintained during the short test. It also assumes that the depth of oxygen penetration in the tailings was infinite, i.e. $C(z, t) = 0$ at $z \rightarrow \infty$. Under these conditions, the evolution of the oxygen concentration C follows the relationship given by Eq. 3 (Elberling et al. 1994).

$$\ln\left(\frac{C}{C_0}\right) = -t\sqrt{K_r D_e} \frac{A}{V} \quad (3)$$

In this equation, A is the area of the air reservoir and V is its volume. The slope of the $\ln(C/C_0)$ versus time t plot provides the value of $(D_e K_r)^{0.5}$. The individual values of K_r and D_e cannot be explicitly determined by this approach. The steady-state oxygen flux into the tailings can be calculated by substituting the term $(D_e K_r)^{0.5}$ in Equation 4 (Elberling et al. 1994, 1996; Mbonimpa et al. 2003).

$$F_s(z=0) = C_0 \sqrt{K_r D_e} \quad (4)$$

Several studies have used this interpretation approach for short OC tests (e.g. Tibble and Nicholson 1997; Elberling and Langdahl 1998; Bussière et al. 2004). Different authors have proposed an alternative approach based on a numerical interpretation, which is also applicable to long duration tests (e.g. Mbonimpa et al. 2000, 2002; 2011; Bussière et al. 2002; Dagenais et al. 2005; Martin et al. 2006; Demers et al. 2009), which are particularly appropriate for relatively low oxygen flux. Dagenais et al. (2012) have also shown how to use this approach to evaluate the oxygen flux through layered covers.

Mbonimpa et al. (2011) have recently shown that this alternative interpretation approach is more representative in many cases, as the conventional interpretation method often tends to underestimate the corresponding flux F_s . One of the main advantages of the numerical interpretation procedure is that it becomes possible to distinguish the values for the two independent parameters D^* and K_r^* (or D_e and K_r) from a single OC test, contrary to the conventional interpretation which only provides a lumped value ($D_e K_r$). The same numerical solutions can also be applied to calculate the oxygen fluxes to the tailings surface, under transient or steady-state conditions.

The value of D_e is known to depend strongly on the volumetric water content θ (or degree of saturation $S_r = \theta / n$); this dependency is represented here using the $D_e(S_r)$ relationship proposed by Aachib et al. (2004), based on the work of Millington and Shearer (1971) and Collin and Rasmuson (1988); this relationship can be written as:

$$D_e = \frac{1}{n^2} \left\{ D_a^0 [n(1-S_r)]^{p_a} + H D_w^0 (n S_r)^{p_w} \right\} \quad (5)$$

In this equation, D_a^0 is the diffusion coefficient of oxygen in air ($\approx 1.56 \text{ m}^2/\text{day}$) and D_w^0 is the diffusion coefficient of oxygen in water ($\approx 2.16 \times 10^{-4} \text{ m}^2/\text{day}$). Precise values for exponents p_a and p_w can be obtained explicitly from the volumetric air and water contents, but in most cases it is sufficient to assume that $p_a = p_w \sim 3.5$.

The value of D_e obtained from Eq. 5 serves to initiate the iterative calculations with POLLUTE to determine the best fit values corresponding to OC test results. To obtain the starting value of K_r , the authors use the simple model proposed by Collin (1987). When the specific surface of the tailings is expressed from the grain-size distribution, this model can be expressed as follows (Mbonimpa et al. 2003; Gosselin et al. 2007).

$$K_r = K' \frac{6}{[1 + 1.17 \log(C_U)] D_{10}} (1-n) C_p \quad (6)$$

where K' is the reactivity of pyrite with oxygen ($K' = 4.33 \times 10^{-5} \text{ m}^3 \text{ O}_2/\text{m}^2 \text{ pyrite}/\text{day}$) and C_p is the pyrite content over mass of dry tailings (kg/kg). One drawback of this model is that it doesn't take into account the influence of S_r on K_r ; this effect is not yet well understood (Gosselin et al. 2007).

Three OC tests were conducted in the field on the tailings surface. Tests 1 and 2 were performed close to trench T-1 and test 3 close to trench T-2. Four tests were made at the base of the trenches: test 4 at the bottom of trench T-1, test 5 at the bottom of trench T-2 and tests 6 and 7 at the bottom of trench T-3. Figure 4 illustrates tests conducted on the tailings surface and at the base of the trenches. The aluminum cylinders used for these tests had an internal diameter of 14.5 cm and a total length of 50 cm. The

reservoir created by placing the lid on top of the cylinder had a height between 1.5 and 4.0 cm. The cylinder was driven into the tailings with a sledge hammer or pushed with a small excavator. The entire system was covered with an insulating box during the tests to limit the effect of varying meteorological conditions. The decrease in oxygen concentration over time within the reservoir was measured using a GC Industry sensor. Another oxygen sensor was left outside the cylinder in the insulating box to monitor the atmospheric concentration during the test; these measurements are used to correct oxygen concentration readings in the source reservoir, which may fluctuate with ambient conditions (Tibble and Nicholson 1997). The water content w , relative density of solid grains D_r , and wet density ρ_{wet} of the tailings were determined and used to evaluate the total porosity n and degree of saturation S_r . As with the laboratory tests, it is assumed that these the tailings characteristics within the cylinder are uniform and constant during a field test.



Figure 4. Images of field OC tests conducted on the tailings surface (left) and at the base of the trenches (right)

Two approaches were used (and compared) for the field tests interpretation: a computational interpretation with the finite element software VADOSE/W (GEO-SLOPE International 2005) and the conventional (analytical-graphical) approach proposed by Elberling et al. (1994, 1996).

The interpretation with VADOSE/W follows somewhat similar lines as with the POLLUTE calculations described above. It is based on an axisymmetric numerical model representing the OC test configuration. Constant values of n and S_r are imposed for the tailings within the cylinder (these parameters are given in Table 2). The volumetric water content at saturation θ_s , considered equal to the measured porosity n , is imposed below the water table. The average volumetric water content θ measured *in situ* is used above the water table. VADOSE uses these hydrogeotechnical characteristics to estimate the value of D^* (and D_e) from the model of Collin and Rasmuson (1988; see also Aachib et al. 2004).

It is assumed also that an equilibrium concentration exists before the start of the test. The estimated value of K_r (based on Equation 6) is used to start the simulation with VADOSE/W (see Mbonimpa et al. 2003, 2011). The oxygen concentration profile at equilibrium in the exposed tailings is obtained from a transient analysis performed over a long period (up to 10 days). The variation of the oxygen concentration in the closed reservoir during the field OC test is then obtained from a new transient simulation, where the equilibrium oxygen profile from the previous step is used as initial condition. The change in oxygen concentration calculated by VADOSE/W is compared with the values measured in the field. Iterative calculations are used to adjust the calculated and measured oxygen concentration curves and thus to obtain the actual (or most representative) value K_r .

Results from Laboratory Tests

Figure 5 shows the result of one of the OC tests performed in the laboratory on the Manitou tailings. The testing period lasted up to 27 days for these tests. Table 1 presents the main characteristics of each test and

the values D_e and K_r resulting from the interpretation with POLLUTE. It is seen that the degree of

saturation S_r of the specimens ranged from 3 to 83% (for a porosity between 0.42 and 0.54). The adjusted

K_r values vary between 0.057d^{-1} and 0.093d^{-1} .

It is seen that the predicted and adjusted values of D_e are very close to each other in all cases, but some significant differences are obtained for K_r .

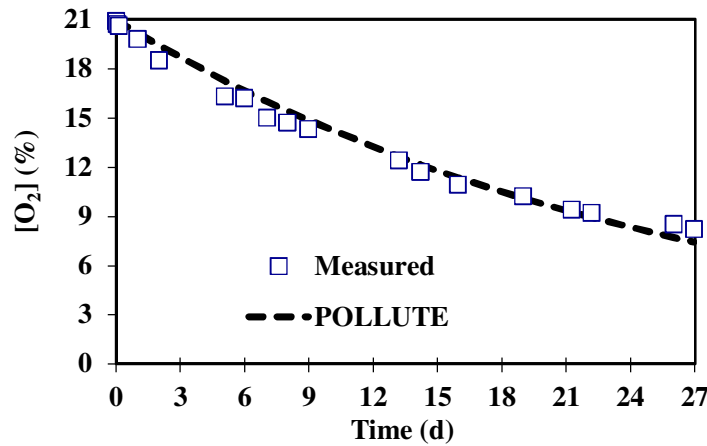


Figure 5. Comparison between the oxygen concentration measured during an OC test on Manitou tailings and those obtained from the numerical calculations with POLLUTE, with adjusted values of D_e and K_r .

Table 1. Characteristics of the laboratory OC tests conducted on the Manitou tailings, with the predicted (pred) and adjusted (adj) values of D_e and K_r .

Test	S_r (%)	n (-)	θ_{eq} (-)	D_{e-pred} (m^2/d)	K_{r-pred} (d^{-1})	D_{e-aj} (m^2/d)	K_{r-adj} (d^{-1})
L1	2.7	0.54	0.53	0.60	0.24	0.59	0.058
L2	10.5	0.44	0.40	0.36	0.29	0.36	0.076
L3	16.8	0.47	0.39	0.31	0.28	0.31	0.094
L4	26.1	0.49	0.36	0.22	0.27	0.22	0.057
L5	37.2	0.47	0.30	0.12	0.28	0.12	0.094
L6	46.3	0.46	0.25	0.074	0.28	0.075	0.16
L7	54.4	0.45	0.21	0.043	0.29	0.043	0.37
L8	63.6	0.42	0.16	0.020	0.30	0.020	0.13
L9	74.4	0.43	0.12	0.007	0.30	0.007	0.056
L10	82.5	0.42	0.08	0.002	0.30	0.002	0.26

Results from Field Tests

Table 2 summarizes the main characteristics of the seven OC tests conducted on the Manitou tailings site. As mentioned above, the porosity n and degree of saturation S_r required for the simulations were obtained from the water content w and the dry density ρ_d measured in field. The value of S_r ranged from 13 to 31% for the surface OC test and from 20 to 30% for the OC test performed at the bottom of the trenches. Figure 6 illustrates the comparison between measured and calculated oxygen concentrations in the reservoir during a test conducted in one of the trenches. It was observed that tests F1 to F3 performed on the surface showed a slower decrease in oxygen concentration than those made in the trenches (Tests F4 to F7).

Table 2 shows that the adjusted values of K_r ranged between 0.0024 d^{-1} and 0.033 d^{-1} for the tests conducted at the surface (tests F1 to F3) and between 0.11 d^{-1} and 1.27 d^{-1} for the tests in trenches (F4 to F7). This difference is deemed to be related to tailings oxidation (and sulphide depletion) close to the surface.

Table 2. Characteristics of the OC tests conducted on the Manitou tailings site, with the predicted (pred) and adjusted (adj) values D_e and K_r .

Test Nr	F1	F2	F3	F4	F5	F6	F7
Location	T-1	T-1	T-2	T-1	T-2	T-3	T-3
Depth (cm)	0	0	0	150	150	180	180
w (%)	18.4	7.8	7.3	10.0	12.2	10.9	10.9
n (-)	0.54	0.51	0.57	0.50	0.41	0.47	0.47
S_r (%)	34.1	15.3	12.8	20.0	29.7	23.2	23.2
θ_{eq} (-)	0.36	0.43	0.50	0.40	0.29	0.36	0.36
D_{e-pred} (m^2/d)	0.170	0.356	0.457	0.288	0.152	0.234	0.234
K_{r-pred} (d^{-1})	-	-	-	0.26	0.31	0.28	0.28
D_{e-adj} (m^2/d)	0.178	0.351	0.457	0.314	0.155	0.195	0.234
K_{r-adj} (d^{-1})	0.033	0.0055	0.0024	1.27	0.11	0.86	0.76

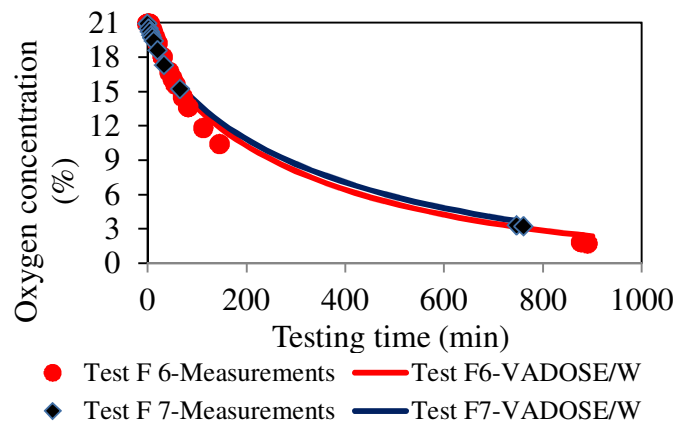


Figure 6. Evolution of the oxygen concentration measured in the reservoir during two OC tests conducted on the Manitou tailings site, with the simulated curves obtained with VADOSE/W for the adjusted value of K_r .

As with the laboratory tests, predicted and adjusted values of D_e are close to each other, while the corresponding values of K_r can be quite different.

Analysis and Discussions

Comparison of K_r values obtained from laboratory and field tests

The results presented above indicate that the values of K_r obtained from the laboratory cell tests using “unoxidized” tailings (sampled at the base of the trenches, with $0.057 \text{ d}^{-1} \leq K_r \leq 0.093 \text{ d}^{-1}$) are lower than those obtained from field tests conducted at the sampling location (F4 to F7). This difference may be due to variations in the tailings characteristics, and also to passivation of the grains surface during sampling and handling. It was observed that these tailings were originally grey when the trenches were excavated, but they took an orange colour within hours when exposed to atmospheric conditions. It was therefore not possible to completely prevent alteration of these tailings before conducting the laboratory tests. This constitutes an additional justification to conduct OC tests in the field.

Figure 7 illustrates how the value of K_r seems to vary with respect to the degree of saturation S_r for the laboratory and field tests results. As the tailings porosity varies from one test to another, the values are normalized (as $K_r/(1-n)$) for comparison purposes. Results from Gosselin et al. (2007) on different tailings indicate that an increase in S_r generally tends to increase $K_r/(1-n)$ at low water content, until a plateau is reached; this trend is not clear from the results obtained herewith the Manitou tailings. The comparison between the values of $K_r/(1-n)$ obtained from the predictive Collin (1987) model (Eq. 6) and the experimental data indicates that the laboratory values are generally lower than the predicted ones. The observed surface alteration may explain this difference, as some passivation of pyrite grains could have reduced the apparent reactivity of these tailings. It is also seen that three of the four values of $K_r/(1-n)$ obtained from the field OC tests conducted in trenches (i.e. F4, F6 and F7) are higher than those predicted by Eq. 6.

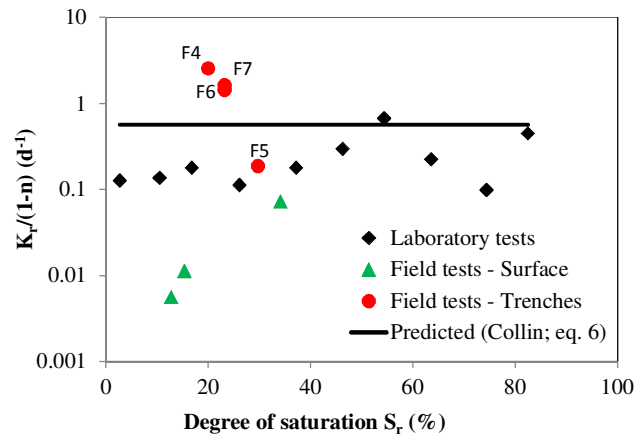


Figure 7. Effect of the degree of saturation on the normalized reaction rate coefficient $K_r/(1-n)$; the values of K_r shown here were obtained from the laboratory using OC tests in closed cells with a single reservoir, and in situ from OC tests on the surface and in trenches.

It is useful to mention here that a complementary OC test was performed in the laboratory using a large column filled with Manitou tailings. Measurements were interpreted with VADOSE/W. The results (not presented in details here) indicated that $K_r/(1-n)$ was about 0.11 d^{-1} for $S_r \approx 0.39$ (Gosselin 2007). This value is close to the results obtained in the laboratory OC tests in closed cells.

Oxygen fluxes

The daily oxygen flux entering in the exposed tailings can be estimated using Equation 4, based on a steady-state hypothesis and assuming that the coefficients D_e and K_r are uniform throughout the tailings. Figure 8 summarizes the oxygen flux results obtained from the laboratory tests (Table 1) and field tests (Table 2).

As expected, the flux would be larger for fresh (unoxidized) tailings exposed to atmospheric conditions, while it would usually be smaller for tailings near the surface that have been preoxidized. The composite laboratory tailings specimens collected at the bottom of the trenches would give intermediate fluxes, and this flux appears to decline when S_r approaches full saturation (which is expected, considering the reduced diffusion coefficient at a large water content).

The field OC tests were also interpreted using the analytical method proposed by Elberling et al. (1994) (Eq. 3). The resulting factors $(D_e K_r)^{0.5}$ were then used to estimate the surface flux with Eq. (4). This flux was compared with the oxygen flux calculated using values D_e and K_r obtained from the numerical interpretation of the field tests. The result of this comparison (not shown here) indicates that the conventional (analytical) interpretation method generally underestimates the flux (for 6 of the 7 field tests), by as much as 80%, confirming other recent results presented by Mbonimpa et al. (2011). Hence, it is deemed more appropriate to interpret the field OC tests using the numerical procedure described briefly above, and presented in more details in Mbonimpa et al. (2002, 2011).

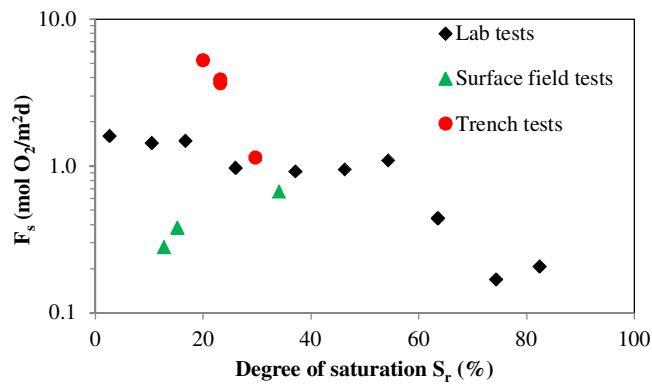


Figure 8. Oxygen fluxes entering exposed tailings, as calculated with Eq. 4 and with the parameters obtained from the laboratory and field OC tests.

Conclusions

Oxygen consumption (OC) tests, as described by Elberling et al. (1994), were performed on the Manitou tailings site at the surface and at the base of three trenches where the tailings were (assumed to be) unoxidized. OC tests were also conducted in closed cells in the laboratory on Manitou tailings samples collected at the bottom of the trenches. Field and laboratory test results were interpreted using numerical simulations. The ensuing diffusion (D_e) and reaction rate (K_r) coefficients were then used to estimate the daily oxygen flux (F_s) entering tailings exposed to the atmosphere. The main findings indicate that the values of K_r (and F_s) obtained from the field tests conducted at the tailings surface are lower than those from tests in trenches; the difference is attributed to the (pre)oxidation of sulphidic minerals close to the surface. The values of K_r (and F_s) obtained from the laboratory tests are larger, but fairly close to those obtained from the field tests performed at the tailings surface; these are lower than those from the field tests performed at the base of the trenches. This would indicate that tailings used in the laboratory tests may have been altered during sampling and preparation (despite the precautions taken in this regard). The K_r values obtained in the trenches also show that the Manitou tailings can be highly reactive, as the reaction rate coefficient measured at depth largely exceeds the value predicted from the pyrite content.

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